

Baindur, S. "Materials Requirements for Nuclear Hydrogen Production Technologies," Canadian Materials Science Conference, CMSC 2007, Hamilton ON, June 2007

Materials Requirements for Nuclear Hydrogen Production Technologies

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Hydrogen Production

- ▶ For Future Transportation Fuel
- ▶ For Current Hydrocarbon Refining
- ▶ For Other Chemical Industry Applications
- ▶ H₂ Production Methods Today:
 - ▶ Separation from
 - Hydrides – Hydrocarbons - e.g. steam reforming of methane
 - Hydrides – Water – e.g. electrical hydrolysis (electrolysis)
 - Heat or electricity required is produced by burning hydrocarbons

Hydrogen Production

- Water Splitting – Hydrolysis – emissions-free if:
 - Electricity or Heat used is produced emissions-free
 - Carbon Dioxide sequestration when commercialized – could yield emissions-free H₂
- Current Emissions-free Energy Options:
 - Solar Thermal Hydrolysis or Electrolysis
 - Wind Powered Electrolysis
 - Low Efficiency and/or Intermittency severe constraints.
 - Nuclear – mature technology unhindered by intermittency issues. Nuclear hydrogen production could use excess power available off-peak hours from NPPs.

Nuclear Hydrogen Production

Nuclear Power Heat (steam) and/or Electricity Enables:

- High Temperature *Thermal* Hydrolysis (thermolysis)
- Thermochemical Hydrolysis
- Electrochemical Processes (including High Temperature Electrolysis, HTE).
- Directed Radiolysis (Hydrogen now produced as waste gas in PWR coolant loop from unintentional radiolysis)

Nuclear Hydrogen Production II

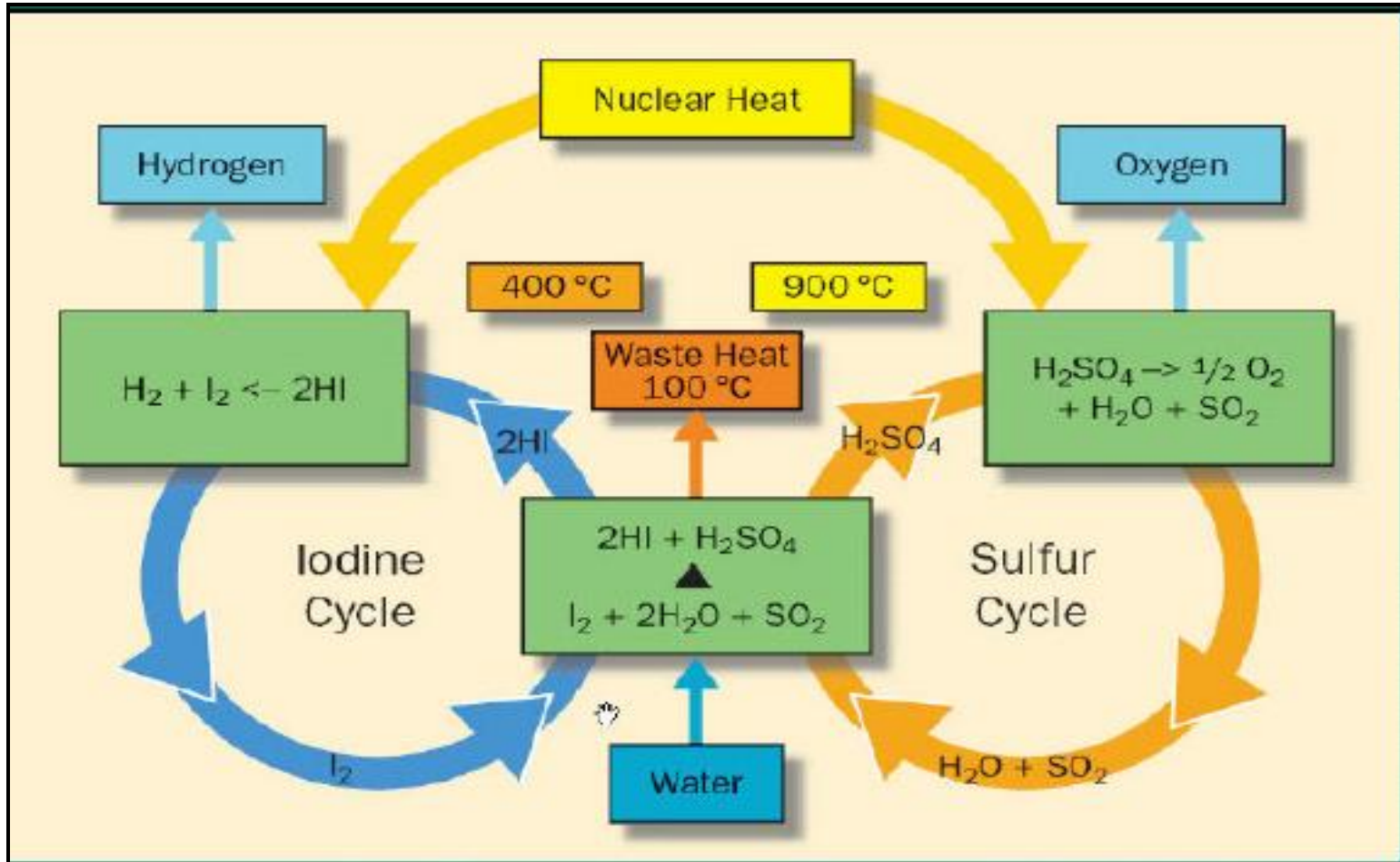
- Dedicated Nuclear Plant for Hydrogen Generation could supply heat and electricity for one or more of the above processes *simultaneously*.
- Next Generation Nuclear Plants will have higher outlet temperatures; thus greater efficiency, both for nuclear plant and for thermo-chemical and electrolytic processes.
- Fifth Generation Nuclear – Fusion – when commercialized – will enable even higher temperatures and production volumes.

Hydrogen Production Options And Their Operating Requirements

	Electrochemical		Thermochemical	
	Water Electrolysis	High Temperature Steam Electrolysis	Steam-Methane Reforming	Thermochemical Water Splitting
Required Temp (Celsius)	< 100, at P _{atm}	>500, at P _{atm}	> 700	> 800 for S-I and WSP > 700 for UT-3 > 600 for Cu-Cl
Efficiency	85 – 90	90 – 95 (at T>800 °C)	> 60, depending on temperature	> 40, depending on TC cycle and temperature
Efficiency w/ Light Water Reactor	~27	~30	Not Applicable	Not Feasible
Efficiency w/ Gas-cooled Reactor (GCR)	>40	>45, depending on power cycle and temperature	> 60, depending on temperature	> 40, depending on TC cycle and temperature
Advantages	+ Proven technology	+ High efficiency + Can be coupled to reactors operating at intermediate temperatures + Eliminates CO ₂ emission	+ Proven technology + Reduces CO ₂ emission	+ Potential for high efficiency + Eliminates CO ₂ emissions
Disadvantages	- Low energy efficiency in the near term	- Requires development of durable, large scale HTSE units	- CO ₂ emissions - Dependent on methane prices	+Aggressive chemistry +Requires very high temperature reactors +Requires development at large scale

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The Sulfur-Iodine (S-I) Thermo-chemical Cycle



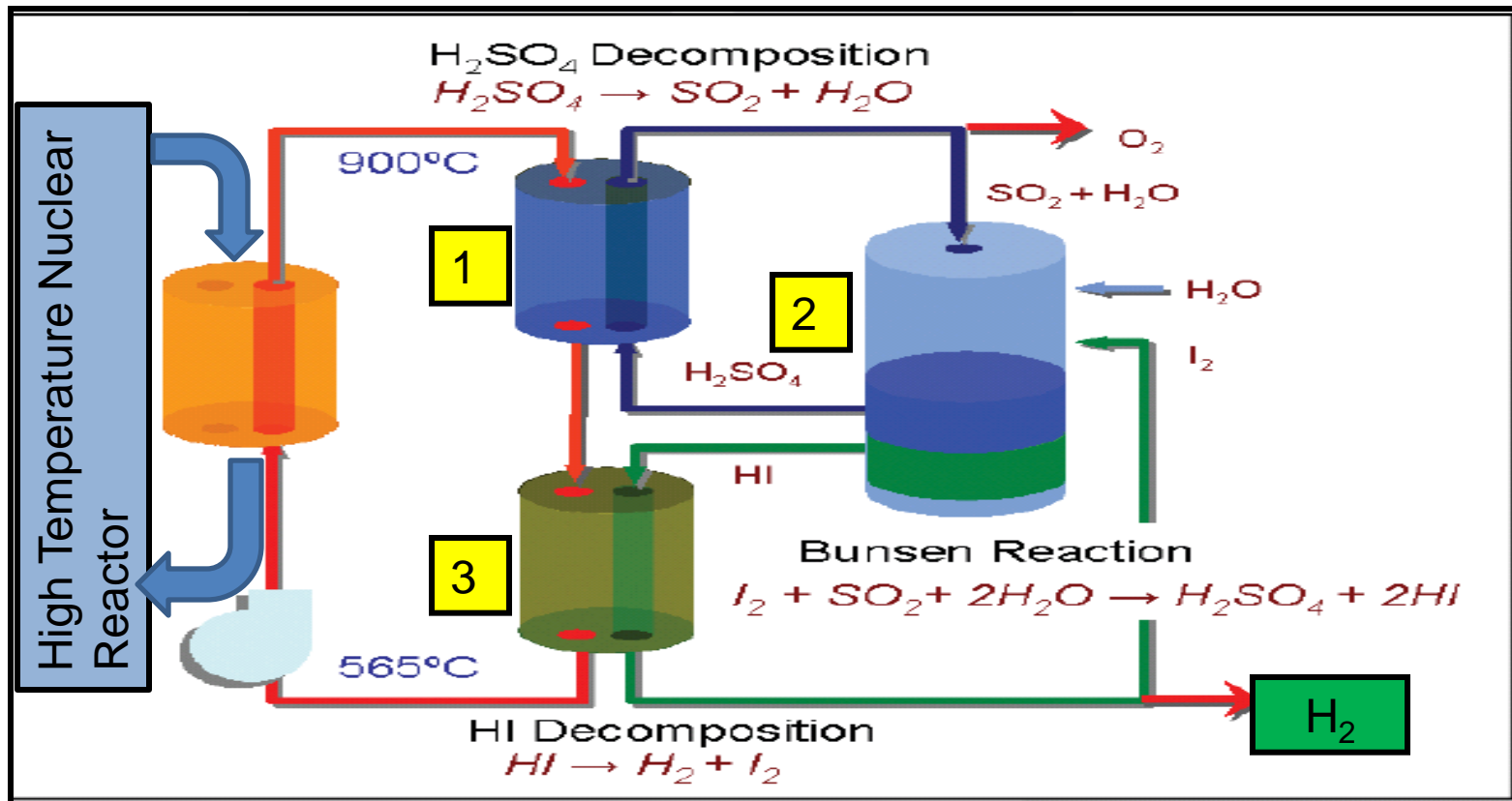
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Other Cycles Being Actively Investigated

- ❖ **NH₃-CO₃-Hg (875-975K)**
- ❖ **Hybrid Cu-Cl (805K)**
- ❖ **Hybrid Cu-SO₄ (1100K)**
- ❖ **Hybrid Zn-SO₄ (1150K)**
- ❖ **NiMnFe (1075K)**
- ❖ **Some new cycles**
 - ◆ **K-Bi (825K)**
 - ◆ **Mg-Cl (875 K)**
 - ◆ **Eu-Br (625 K) (recently identified)**

Wilson, Corwin, Sherman, Pickard (2006)

Schematic of the 3 Major Components of a Nuclear Hydrogen Production Facility



Adapted from Wang (2006)

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Basic R&D Issues in High Temp T-C Hydrogen Production Cycles

- ▶ Scaling and Efficiency are the Main Issues for thermochemical cycles – bench to pilot plant to industrial scale
- ▶ But T-C Cycles Also Present Very Demanding Thermal Management Challenges during Operation.
- ▶ Materials Challenges Include:
 - ▶ High-temperature Resistance (alloys, ceramics or refractories)
 - ▶ Chemical Corrosion Resistance (against acids)
 - ▶ Stress Corrosion Resistance (from high Pressure and Temperature conditions)
 - ▶ Materials Challenges serious: cause Viability Concerns. (also see Baidur 2007a).

Candidate Materials for S-I Cycle (Wang 2006)

- Sulfuric Acid Decomposition
 - Outputs Oxygen and Sulfur Dioxide
 - Alloy 800 and Hastelloys for Reaction Vessel and Piping; also Ceramics
- Bunsen Reaction
 - Produces Hydrogen Iodide and Sulfuric Acid
 - Fe-Si Alloys work well as Reaction Vessels and Concentrators;
- Hydrogen Iodide Decomposition
 - Produces and Separates Hydrogen and Iodine
 - Tantalum and Wolfram (Tungsten) Alloys best corrosion resistance
- Extensive Testing of Candidate Materials Required to move beyond Bench Scale

Heat Exchanger Candidate Materials (Hechanova UNLV 2005)

- Tensile Property Tests of 3 Nickel-based Alloys: C-22, C-276 and Waspalloy are ongoing at UNLV at (i) Ambient Temperature (ii) 450 C and (iii) 600 C in a nitrogen atmosphere.
- Stress Corrosion Cracking (SCC) for above 3 alloys also measured in 90 C aqueous solution of sulfuric acid and sodium iodide at (i) constant load (ii) slow strain-rate.
- Incoloy-800 also tested for SCC and tensile strength at UNLV
- MIT has tested alloys 800HT and 617 for Heat Exchanger with Catalyst Platinum (Pt) in 2-30 %wt for Sulfuric Acid Decomposition. (Hechanova 2005)

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